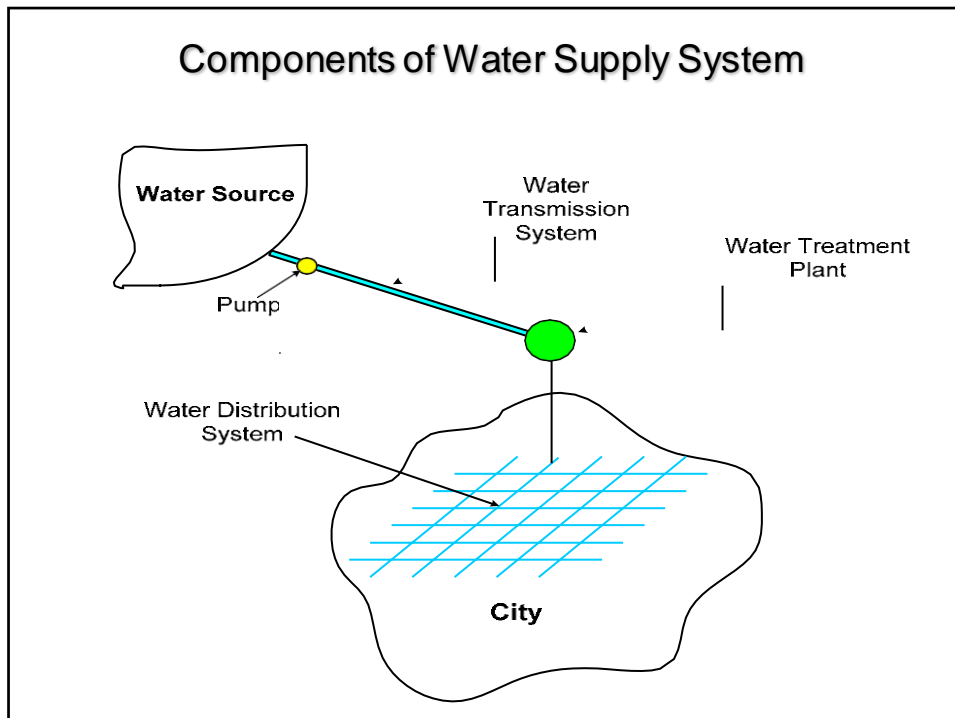


# **WATER DISTRIBUTION NETWORKS and Design**

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## **Water Distribution System**

- Water distribution systems are designed to adequately satisfy the water requirements for a combinations of the following demands:
  - Domestic
  - Commercial
  - Industrial
  - Fire-fighting
  
- The system should be capable of meeting the demands at all times and at satisfactory pressure

## **Water Distribution System**

- The main elements of the distribution system are:
  - Pipe systems
  - Pumping stations
  - Storage facilities
  - Fire hydrants
  - House service connections
  - Meters
  - Other appurtenances

## System Configurations

➤ Distribution systems may be classified as:

- Branching systems
- Grid systems
- A combination of the above two systems

➤ The configuration of the system is dictated by:

- Street patterns
- Topography
- Degree and type of development of the area
- Location of the treatment and storage works.

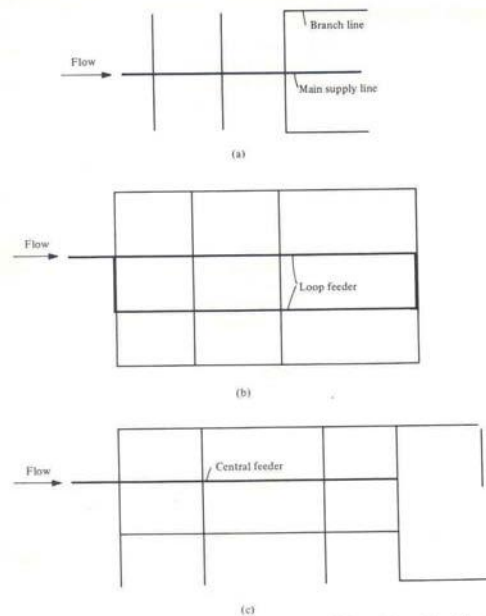


Figure 6.4 Types of water distribution systems: (a) Branching, (b) grid, and (c) combination.

## **System Configurations**

### ➤ Branching vs. grid systems:

- A grid system is usually preferred over a branching system, since it can furnish a supply to any point from at least two directions
- The branching system has dead ends, therefore, does not permit supply from more than one direction. Should be avoided where possible.
- In locations where sharp changes in topography occur (hilly or mountainous areas), it is common practice to divide the distribution system into two or more service areas.

## **Basic System Requirements**

### ➤ Pressure:

- Pressure should be great enough to adequately meet consumer and fire-fighting needs.
- Pressure should not be excessive:
  - Cost consideration
  - Leakage and maintenance increase

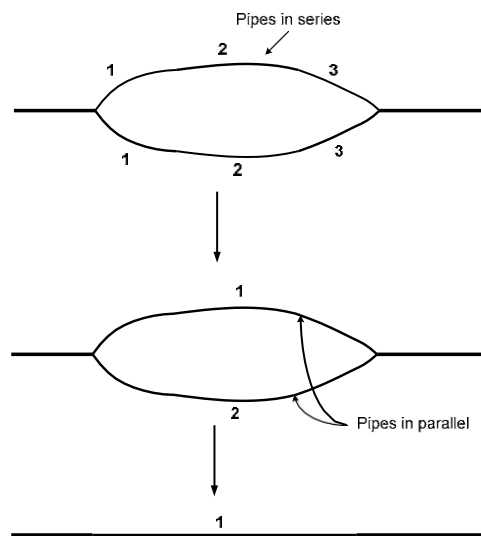
### ➤ Capacity:

- The capacity is determined on the bases of local water needs plus fire-fighting demand.
- Pipe sizes should be selected to avoid high velocities:
  - Pipe sizes should have selected based on flow velocity of 3-5 fps
  - Where fire-fighting is required, minimum pipe diameter is 6 in.

## Hydraulic Design

- The design flowrate is based on the maximum of the following two rates:
  - Maximum day demand plus fire demand
  - Maximum hourly rate
- Analysis of distribution system:
  - Distribution system have series of pipes of different diameters. In order to simplify the analysis, skeletonizing is used.
  - Skeletonizing is the replacement of a series of pipes of varying diameters with one equivalent pipe or replacing a system of pipes with one equivalent pipe.

### Skeletonization



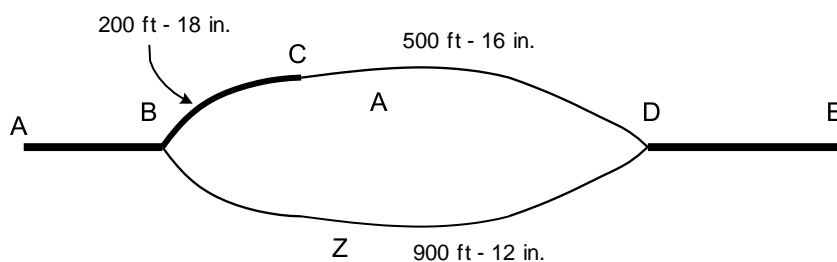
## Hydraulic Design

### ➤ Example:

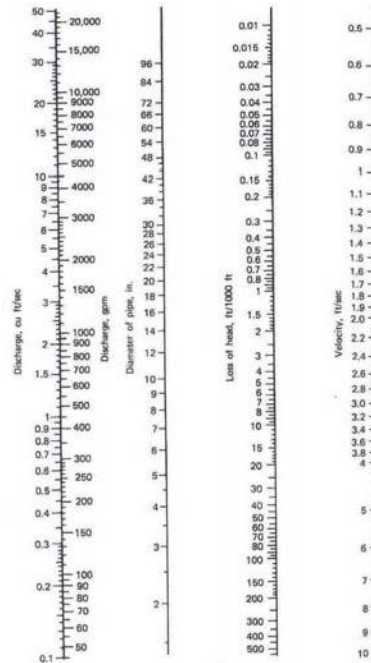
Consider the piping system shown in the figure, replace (a) pipes BC and CD with an equivalent 12-in. pipe and (b) the system from B to D with an equivalent 20-in. pipe.

### ➤ Solution:

- a) for pipes in series:
  1. assume any value for Q through BCD (8 cfs)
  2. from nomograph with  $Q = 8$  cfs and dia = 18-in, read head loss for BC = 6.1ft/1000ft
  3. from nomograph with  $Q = 8$  cfs and dia = 16-in, read head loss for CD = 11ft/1000ft
  4. total head loss BD =  $(6.1/1000)*200+(11/1000)*500 = 6.72$ ft



Nomograph for Hazen  
Williams equation



## Hydraulic Design

5. the total head loss for 12-in equivalent pipe at 8 cfs is 45ft/1000ft (from nomograph)

6. head loss BCD = head loss BD, therefore;

$$6.72\text{ft} = L_{\text{eq}} * (45/1000)$$

$$L_{\text{eq}} = 6.72 * (1000/45) = 149 \text{ ft}$$

- b) for pipes in parallel:

1. assume any value of head loss between BD ( $h_L=5 \text{ ft}$ )

2. for the equivalent pipe ( $L = 149 \text{ ft}$ ), head loss per 1000ft is;

$$h_L = (5/149)*1000 = 33.5\text{ft}/1000\text{ft}$$

Diameter of equivalent pipe = 12-in

$$Q_{\text{eq}} = 6.8 \text{ cfs (from nomograph)}$$

## Hydraulic Design

3. for the 900 ft 12-in pipe:

$$h_L = (5/900) * 1000 = 5.5 \text{ ft}/1000 \text{ ft}$$

$$Q_{900} = 2.6 \text{ cfs (from nomograph)}$$

4. total flow = 6.9 + 2.6 = 9.4 cfs

5. for Q = 9.4 cfs and 20-in pipe:

$$\text{head loss} = 4.8 \text{ ft}/1000 \text{ ft} \quad (\text{nomograph})$$

6. head loss 12-in pipe = head loss 20-in pipe

$$5 \text{ ft} = L * (4.8 \text{ ft}/1000 \text{ ft})$$

$$L = 5 * (1000/4.8) = 1042 \text{ ft}$$

## Hydraulic Design

### ➤ Pipe networks:

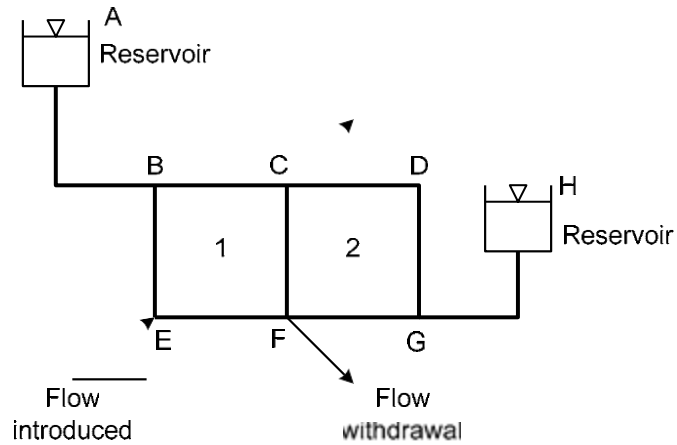
- Pipe networks are composed of a number of constant-diameter pipe sections containing pumps and fittings.
- From next figure, following are defined:
  - Node: end of each pipe section. (A, B, C, D, E, F, G, and H)
  - Junction node: points where pipes meet and where flow may be introduced or withdrawn. (B, C, D, E, F, and G)
  - Fixed-grade nodes: points where constant grade is maintained. (A and B)
  - Loops: closed pipe circuits. (1 and 2)
- From above terminology, we can write the following eq.

$$P = J + L + F - 1$$

Where: P = # pipes, J = # Junction node, L = #loops,  
F = # fixed-grade nodes



## Pipe Network



## Hydraulic Design

### ➤ Loop equations:

- Hydraulic performance of pipe networks are based on mass continuity and energy conservation.

- Continuity of mass:**

$$\Sigma Q_{in} - \Sigma Q_{out} = Q_e \text{ (J number of equations)}$$

$Q_{in}$  = inflow into node

$Q_{out}$  = outflow from node

$Q_e$  = external flow into the system or withdrawal

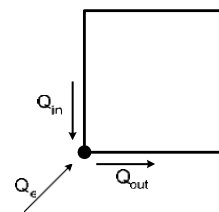
- Conservation of energy:**

$$\Sigma h_L = \Sigma E_p \text{ (L number of equations)}$$

$h_L$  = head loss;  $E_p$  = pump head

For fixed-grade nodes, the following can be written:

$$\Delta E = \Sigma h_L - \Sigma E_p \text{ (F-1 equations)}$$



## Hydraulic Design

### ➤ Loop equations: (continue)

- **Frictional losses in pipes:**

$$h_{LP} = K_p Q^n$$

Where;

$K_p$  = constant incorporating pipe size, its roughness, and units used

$n$  = an exponent

The Hazen-Williams formula for head loss is given as:

$$h_{LP} = K_p Q^{1.85}$$

- **Minor losses:**

These losses are due fittings, valves, meters, or other insertions that affect the flow. They are expressed as:

$$h_{LM} = K_M Q^2$$

Where;

$K_M$  = minor loss constant

## Hydraulic Design

### ➤ Node equations:

- When considering nodes, the principle relationship used is the continuity equation:

$$Q_{in} - Q_{out} = Q_c$$

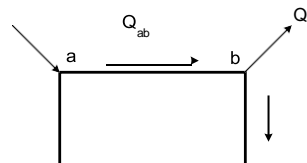
- The discharge in pipe ab can be expressed in terms of grade (head) as the following:

$$h_L = KQ^n$$

$$h_{Lab} = h_a - h_b = K_{ab} Q^n$$

Or

$$Q_{ab} = \{(h_a - h_b) / K_{ab}\}^{1/n}$$



## Hydraulic Design

### ➤ Node equations:

- If pump exist in the line, then junction nodes are specified at the inlet and outlet.



for continuity:

$$Q_{ab} = Q_{cd}$$

$$\{(h_a - h_b)/K_{ab}\}^{1/n} = \{(h_c - h_d)/K_{cd}\}^{1/n}$$

$$h_a - h_b = (K_{ab}/K_{cd}) (h_c - h_d)$$

The head change across pump is:

$$h_c - h_b = P(Q)$$

$P(Q)$  = is the head developed by the pump =  $(550 \text{ hp})/(\gamma Q)$

hp = horsepower,  $\gamma$  = weight of water,  $Q$  = flow

## Distribution Reservoirs

### ➤ Definition:

Distribution reservoirs provide service storage to meet the widely fluctuating demands often imposed on the distribution system, to accommodate fire-fighting and emergency requirements, and to equalize operating pressure.

### ➤ Types of reservoirs:

- **Surface reservoir**
  - Usually lined with concrete, gunite, asphalt, or membrane.
  - They may be covered or uncovered, but usually covered to prevent contamination.
- **Standpipes or elevated tanks**
  - Normally employed where the construction of a surface reservoir would not provide sufficient head.
  - Stand pipes are tall cylindrical tanks whose storage volume includes an upper portion (useful storage) and a lower portion (supporting storage).



Surface Reservoir



Standpipes

## Elevated tanks



## Distribution Reservoirs

### ➤ Location

- Distribution reservoirs should be located strategically for maximum benefits.
- Normally the reservoir should be near the center of use.
- For large areas, a number of reservoirs may be located at key locations
- A central location decreases the friction losses by reducing the distance to the serviced area.

### ➤ Storage function

- To provide head required head.
- To provide excess demand such as:
  - fire-fighting: should be sufficient to provide flow for 10-12 hours.
  - emergency demands: to sustain the demand during failure of the supply system and times of maintenance.
- To provide equalization storage.

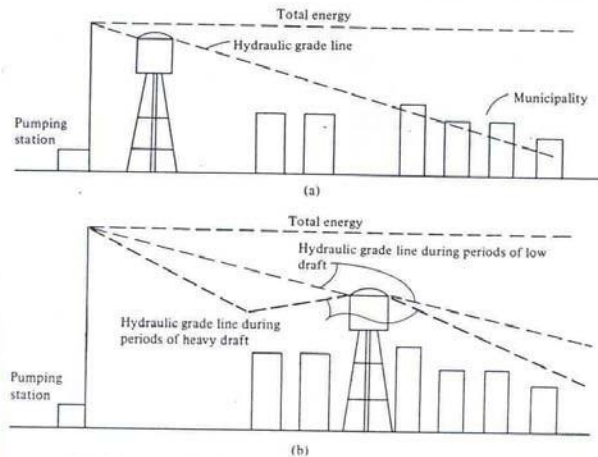


Figure 6.20 Pressure distribution as influenced by the location of a distribution reservoir.

## Pumping

### ➤ Introduction

- Pumping is an important part of the transportation and distribution system.
- Requirements vary from small units (few gallons per minute) to large units (several hundred cubic feet per second)
- Two kinds of pumping equipments are mainly used; centrifugal and displacement pumps.

### ➤ Types of pumps

- **Low-lift pumps:** used to lift water from a source to the treatment plant
- **High-service pumps:** used to discharge water under pressure to the distribution system
- **Booster pumps:** used to increase pressure in the distribution system.
- **Recirculation pumps:** used within a treatment plant.
- **Well pumps:** used to lift water from wells.

## Centrifugal pumps

- Used to lift and transport water
- Widely used in water and wastewater applications due to:
  - Simplicity of installation and operation.
  - Compactness.
  - Low cost compared to others.
  - Operate under variety of conditions
- How do they operate:
  - On the principle of centrifugal force; force of pushing outwards.
  - The impeller driven at high speed throws water into the casing
  - Water is channeled through a nozzle to the discharge piping

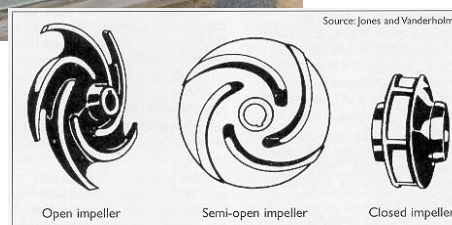
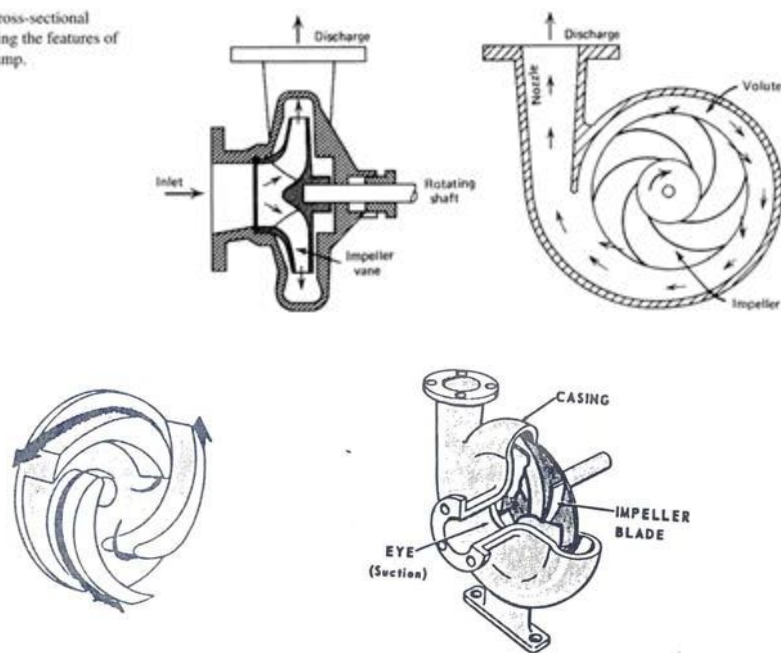


Figure 1. Common impeller types for centrifugal pumps.

**Figure 4-9** Cross-sectional diagrams showing the features of a centrifugal pump.



## Centrifugal pumps

### ➤ Pumping head

- The pump operates against a certain head called Total Dynamic Head (TDH).
- TDH is composed of the following:
  - The difference in elevation between the pump centerline and the elevation to which the water is to be raised.
  - The difference in elevation between the level of the suction pool and the pump centerline
  - The friction losses
  - Velocity head

$$\mathbf{TDH = H_L + H_f + H_v}$$

Where;

$H_L$  = total static head

$H_f$  = total friction head

$H_v$  = velocity head ( $V^2/2g$ )



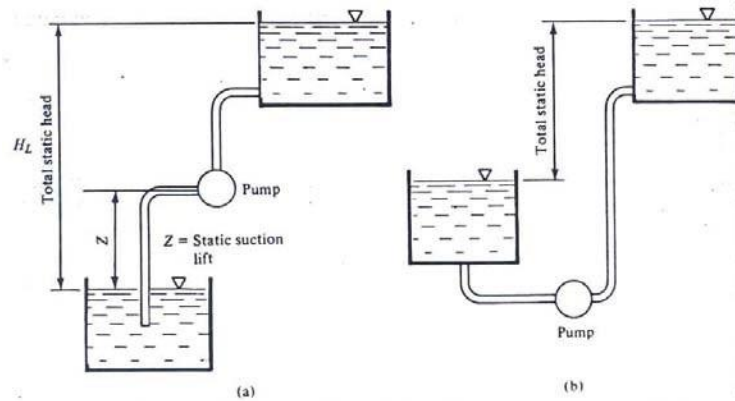


Figure 6.25 Total static head: (a) Intake below the pump centerline and (b) intake above the pump centerline.

## Centrifugal pumps

### ➤ Power

- The theoretical horsepower required may be found by using the following equation:

$$hp = Q\gamma H/550$$

Where;

Q = discharge, cfs

$\gamma$  = specific weight of water, 62.4 lb/ft<sup>3</sup>

H = total dynamic head, ft

The actual hp required is obtained by dividing the theoretical hp by the efficiency of the pump.

## Centrifugal pumps

### ➤ System head

- The system head is represented by a plot of TDH vs. discharge for the system being studied.
- The plot is used to help in selecting the pumping unit.
- The system head curve will vary with flow since  $H_F$  and  $H_V$  are both a function of discharge.
- Since the static head  $H_L$  may vary as a result of fluctuating water levels, it is necessary to plot system head curves covering the range of variations in static head.

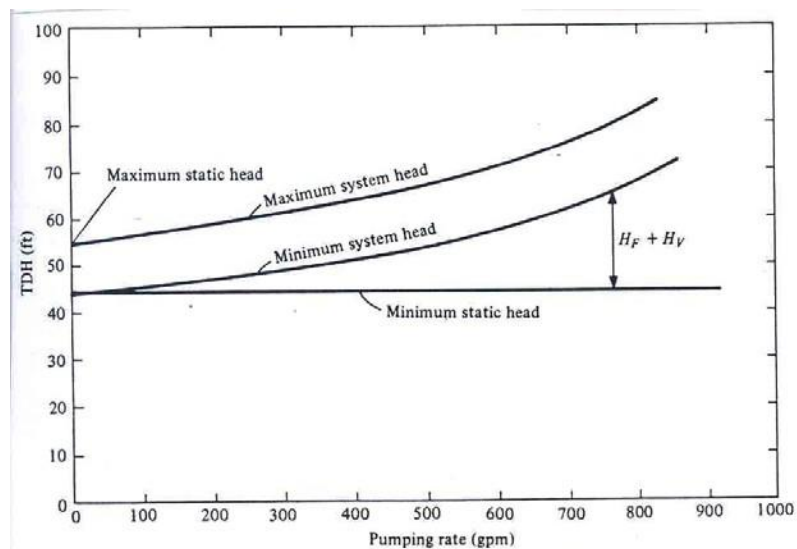


Figure 6.26 System head curves for a fluctuating static pumping head.

## Centrifugal pumps

### ➤ Pump characteristics

- Each pump has its own characteristics relative to power requirements, efficiency, and head developed as a function of rate of flow.
- These relationships are usually given as a set of pump characteristic curves for a specified speed.
- Pump characteristic curves are used in conjunction with system-head curves to select suitable pumping equipment for a particular installation.
- As the flow of the centrifugal pump increases, the head will fall.
- At maximum efficiency, the discharge is known as *normal* or *rated discharge*.
- To change the flow, the practical and efficient approach is to provide two or more pumps in parallel so that the flow may be carried at close to the peak efficiency.
- The normal range of efficiency is between 50-85%.

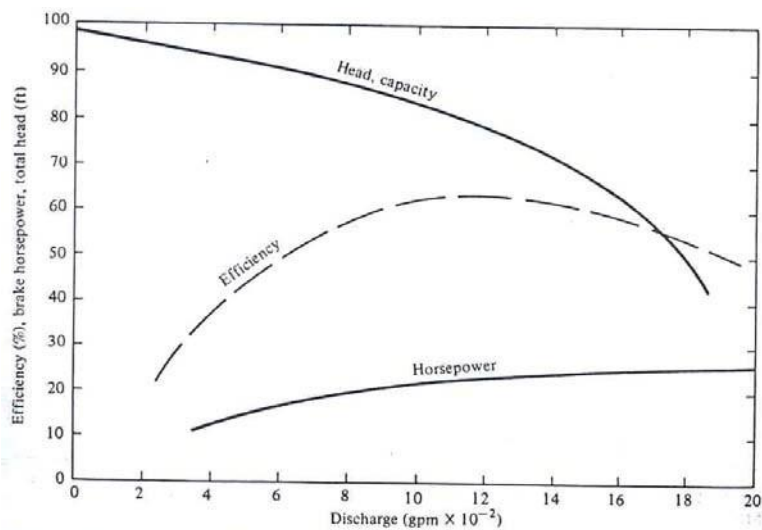
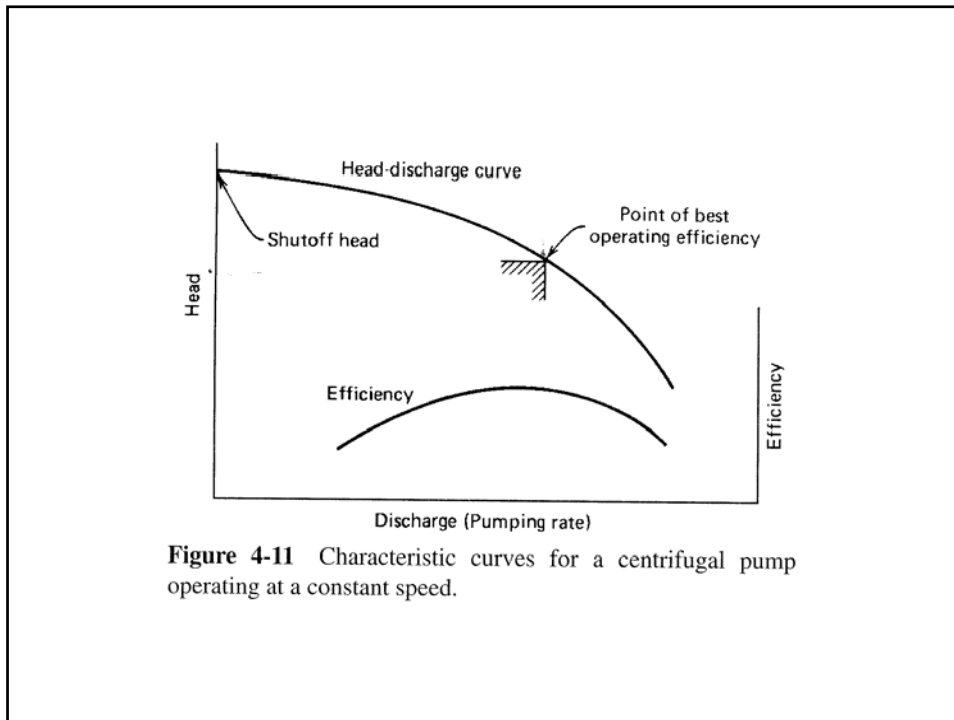


Figure 6.27 Typical pump characteristic curves.



**Figure 4-11** Characteristic curves for a centrifugal pump operating at a constant speed.

## Centrifugal pumps

### ➤ Selection of pumping units

- Normally the engineer is given the system-head characteristics curve and is required to find a pump or pumps to deliver the required flow.
- The system-head curve is plotted with the pump characteristics curve.
- The operating point is located at the intersection of the system-head curve and the pump characteristics curve. This point gives the head and flow at which the pump will be operating.
- A pump should be selected so that the operating point is also as close as possible to peak efficiency.
- Pumps connected in series; the total head equals the sum of the heads added by each pump (discharge stay constant).
- Pumps connected in parallel; the total discharge is the sum of the discharges of each pump at a given head (head stay constant).

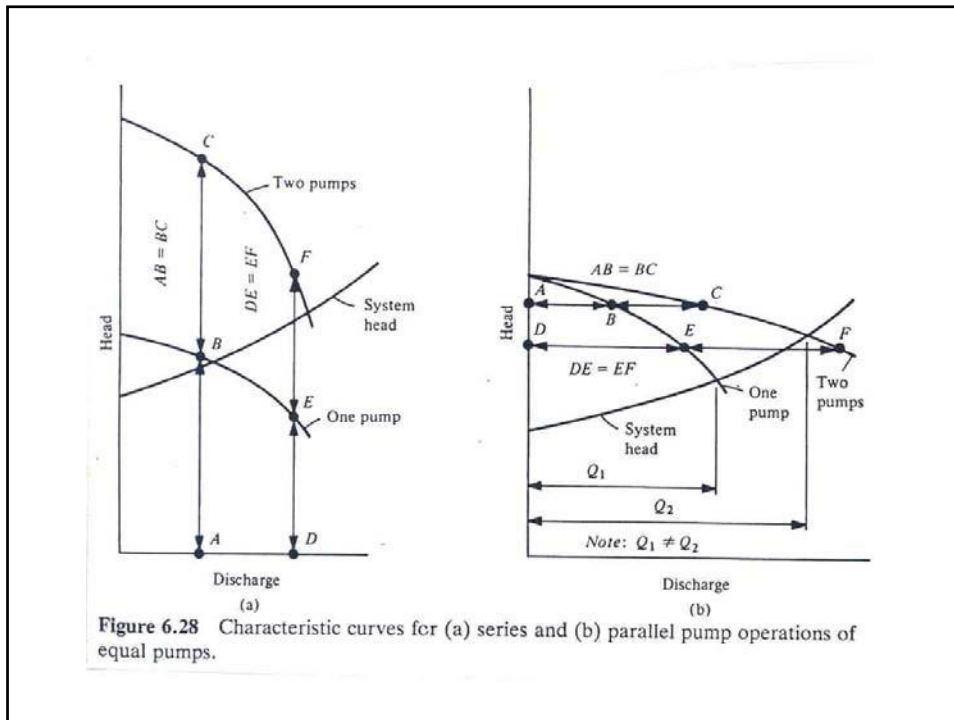


Figure 6.28 Characteristic curves for (a) series and (b) parallel pump operations of equal pumps.

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